

4 Frederking, T. H. K., "Remarks on the Heat Transfer in Helium II at High Flux Values," UCLA Department of Engineering, Report No. 62-5, 1962, p. 22.

5 Goodling, J. S., and Irey, R. K., "Non-Boiling and Film Boiling Heat Transfer to a Saturated Bath of Liquid Helium," *Advances in Cryogenic Engineering*, Vol. 14, Plenum Press, New York, 1969, p. 159.

6 Rivers, W. J., and McFadden, P. W., "Film Free Convection in Helium II," *JOURNAL OF HEAT TRANSFER, TRANS. ASME, Series C*, Vol. 88, No. 4, November 1966, pp. 343-350.

7 Rivers, W. J., "An Analytical Investigation of Film Free Convection Heat Transfer to Liquid Helium II," PhD thesis, Purdue University, Lafayette, Indiana, 1964.

8 Holdredge, R. M., "Heat Transfer From Cylinders to a Saturated Liquid Helium II Bath," PhD thesis, Purdue University, Lafayette, Indiana, 1965.

9 McFadden, P. W., and Holdredge, R. M., "Heat Transfer to a Saturated Bath of Liquid Helium II," *Heat Flow Below 100 Deg K and Its Technological Applications*, Institut International du Froid and Pergamon Press, Paris, 1965, p. 259.

10 Frederking, T. H. K., "Waermeuebergang bei der Verdampfung der verfluessigten Gas Helium and Stickstoff," *Forschung auf dem Gebiete des Ingenieurwesens*, Vol. 27, 1961, p. 17.

11 Frederking, T. H. K., Personal Communication.

12 Bromley, L. A., "Heat Transfer in Stable Film Boiling," *Chemical Engineering Progress*, Vol. 46, May 1950, p. 221.

13 Breen, B. P., and Westwater, J. W., "Effect of Diameter of Horizontal Tubes on Film Boiling Heat Transfer," *Chemical Engineering Progress*, Vol. 58, July 1962, p. 67.

14 McFadden, P. W., "An Analytical Investigation of Laminar Film Boiling," PhD thesis, Purdue University, Lafayette, Indiana, 1959.

15 Hermann, R., "Waermeuebertragung bei freier Stroemung am waagerechten Zylinder in zwei-atomigen Gasen," *VDT-Forschungsheft*, No. 379, Berlin, 1936.

DISCUSSION

T. H. K. Frederking³

The authors' classification of heat transfer regimes in superfluid He II appears to be quite useful when the region of large heat flux densities is considered. It is noted however, that the definition of regime 2 (Fig. 2) may not be generally acceptable in the light of the experiments of reference [5] and others. In other experiments [5] the establishment of several cooling curves in regime 2 (instead of one single function) is less obvious. In this context, it is noted that the present specimen geometry has been adopted also by Efferson.⁴ Efferson's results show that the particular combination of specimen materials allows large temperature fluctuations at high heat fluxes. This point deserves attention since in cryogenic technology equipment these conditions appear to be more frequent than perfect temperature uniformity.

The major point of concern in the present paper is the applicability of the Rivers-McFadden model to He II film boiling. It is

³ University of California, Los Angeles, Calif.

⁴ Efferson, K. R., "Heat Transfer From Cylindrical Surfaces to Liquid He I," *Journal of Applied Physics*, Vol. 40, 1969, p. 1995.

known that film boiling of subcooled liquids, aside from vapor film properties, is affected by the conditions in the liquid (stirring, forced convection, stratification). These effects shift the numerical values of the thermal conductances. Usually, however, the order of magnitude is not altered. Similarly, in film boiling of He II the heat transfer is influenced by the state of the liquid (bath temperature, liquid heat path), as demonstrated in Fig. 7 of the paper. In contrast to ordinary subcooled film boiling however, the thermodynamic conditions in the He II have not yet been resolved completely. Therefore, the related thermohydrodynamics has not yet been cast into forms which allow more detailed calculations of the present problem. In view of this state of the art, Rivers and McFadden displayed considerable intuition when they adopted the profiles of Fig. 4 for their integral treatment. As long as the range of validity of these profiles cannot yet be fully assessed, the Rivers-McFadden model gives (as documented in Fig. 10) a remarkable account of film boiling heat transfer in He II.

Authors' Closure

The authors would like to thank Dr. Frederking for his comments and for his analysis of the problems associated with film boiling in He II. In considering regime 2 (Fig. 2) two items should be kept in mind. First, Fig. 2 is intended as a qualitative representation and care should be taken in attaching quantitative significance. Second, Goodling and Irey [5] state,

As noted in Figs. 2 and 3, the experimental data begins to deviate from the Khalatnikov theory at a heat flux on the order of 0.1 W/cm² and diverges by as much as 35% in the vicinity of the peak flux. This agrees with the data reported by Holdredge and McFadden [13].

Dr. Frederking's comments substantiate the statement in the text expressing the need for more results to confirm and describe this region.

The test section used by Efferson was somewhat different in that no provision was made to insure minimum thermal contact with the ends of the test section by way of the thermometer leads. Also, in using test sections of this design a match of thermal expansion between the film and glass is important. Helium I data were taken with the test sections used in this investigation, and the results⁵ do not show the fluctuation noted by Efferson. However, Dr. Frederking's comments concerning the need for investigation in material combinations where large temperature fluctuations occur at high heat fluxes does point out a problem area.

⁵ Holdredge, R. M., and McFadden, P. W., "Heat Transfer From Horizontal Cylinders to a Saturated Helium I Bath," Paper G-5, 1970 Cryogenic Engineering Conference, June 1970, Boulder, Colo., to be published in Vol. 16 of *Advances in Cryogenic Engineering*.